Numerical Simulation of Red Blood Cell Suspensions Behind a Moving Interface in a Capillary

Shihai Zhao and Tsorng-Whay Pan*

Department of Mathematics, University of Houston, Houston, Texas 77204, USA.

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Abstract. Computational modeling and simulation are presented on the motion of red blood cells behind a moving interface in a capillary. The methodology is based on an immersed boundary method and the skeleton structure of the red blood cell (RBC) membrane is modeled as a spring network. As by the nature of the problem, the computational domain is moving with either a designated RBC or an interface in an infinitely long two-dimensional channel with an undisturbed flow field in front of the computational domain. The tanking-treading and the inclination angle of a cell in a simple shear flow are briefly discussed for the validation purpose. We then present and discuss the results of the motion of red blood cells behind a moving interface in a capillary, which show that the RBCs with higher velocity than the interface speed form a concentrated slug behind the moving interface.

AMS subject classifications: 65M60, 76M10, 76Z05 **Key words**: Red blood cells, moving domain, immersed boundary method.

1. Introduction

The rheological property of the red blood cells (RBCs) is a key factor of the blood flow characteristics at the microchannel level, especially the particulate nature of the blood becomes significant when studying blood drop through a glass capillary within miniature blood diagnostic kit. The penetration of the blood suspension in a perfectly wettable capillary has been analyzed in [1, 2]. The failure of such penetration is attributed to three RBCs segregation mechanisms: (i) corner deflection at the entrance, (ii) the intermediate deformation-induced radial migration and (iii) shear-induced diffusion within a packed slug at the meniscus. The key mechanism responsible for penetration failure is the deformation-induced radial migration, which endows the blood cells with a higher velocity than the meniscus to form the concentrated slug behind the

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^{*}Corresponding author. Email addresses: shhzhao@math.uh.edu (S. Zhao), pan@math.uh.edu (T.-W. Pan)

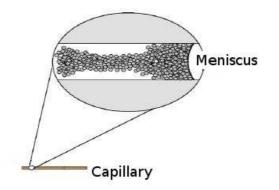


Figure 1: Schematics of the BRCs moving behind a meniscus.

meniscus (see Fig. 1). The results in [1,2] shed light on making the smallest microfluidic kit and loading microneedle that require the least amount of blood sample.

Nowadays in silico mathematical modeling and numerical study of RBC rheology have attracted growing interest (see, e.g., [3, 4]). The immersed boundary method developed by Peskin, e.g., [5–7], has been one of the popular methodologies for numerically studying the RBC rheology due its distinguish features in dealing with the problem of fluid flow interacting with a flexible fluid/structure interface. For example, in [8-17], immersed boundary methods have been combined with different RBC membrane models to simulate the motion of RBCs and vesicles in fluid flow. We have successfully combined an immersed boundary method with a spring model developed in [18] to simulate the motion of RBCs in shear flows and Poiseuille flows in [15–17]. To simulate the RBCs aggregation behind a moving interface considered in [1, 2], we have extended the aforementioned methodology since the typical setting of the periodic boundary condition in the channel wall direction is not well suited anymore. As by the nature of the problem, the computational domain has to be focused on the marching frontier, which has no counterpart to go periodic. Instead we have the computational domain moving with a interface (see, e.g., [26, 27] and references therein for adjusting the computational domain) in an infinitely long two-dimensional channel with an undisturbed flow field in front of the domain. This approach extends the range of the methodology from still focus to moving focus. To mimic the motion of the RBCs behind a meniscus in a capillary, we have considered a flat interface moving with a given constant speed in this paper. The simulating results of the motion of red blood cells behind a moving interface show that the RBCs with higher velocity in the channel central region than the interface speed form the concentrated slug behind the interface, which resembles the motion of the RBCs observed in [1,2]. The structure of this paper is as follows: We discuss the elastic spring model and numerical methods in Section 2. In Section 3, the tanking-treading and the inclination angle of a cell in a simple shear flow are briefly discussed for the validation purpose. We then present and discuss the results of the motion of red blood cells behind a moving interface in a capillary. The conclusions are summarized in Section 4.

2. Models and methods

Let Ω be a bounded rectangular domain filled with blood plasma which is incompressible, Newtonian, and contains RBCs with the viscosity of the cytoplasm same as that of the blood plasma (see Fig. 2). For some T > 0, the governing equations for the fluid-cell system are

$$\rho \left[\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right] = -\nabla p + \mu \Delta \mathbf{u} + \mathbf{f} \quad \text{in } \Omega, \ t \in (0, T),$$
(2.1)

$$\boldsymbol{\nabla} \cdot \mathbf{u} = 0 \quad \text{in } \Omega, \quad t \in (0, T), \tag{2.2}$$

where **u** and *p* are the fluid velocity and pressure, respectively, ρ is the fluid density, and μ is the fluid viscosity, which is assumed to be constant for the entire computational domain. In (2.1), **f** is a body force which accounts for the force acting on the fluid/cell interface. Eqs. (2.1) and (2.2) are completed by the following boundary and initial conditions:

$$\mathbf{u} = \mathbf{g}_0 \quad \text{on} \ \Gamma_d, \tag{2.3}$$

$$\mu \frac{\partial \mathbf{u}}{\partial \mathbf{n}} - \mathbf{n}p = \mathbf{0} \quad \text{on } \Gamma_n, \tag{2.4}$$

$$\mathbf{u}(0) = \mathbf{u}_0,\tag{2.5}$$

where the domain Ω is taken from an infinitely long channel with its boundary denoted by $\Gamma = \bigcup_{i=1}^{4} \Gamma_i$. In the simulations, we have considered two types of boundary conditions: (i) $\Gamma_n = \emptyset$ and $\Gamma_d = \Gamma$, (ii) $\Gamma_n = \Gamma_4$ and $\Gamma_d = \Gamma_1 \cup \Gamma_2 \cup \Gamma_3$ with \mathbf{g}_0 having the profile of either Poiseuille flow or simple shear flow on Γ_d .

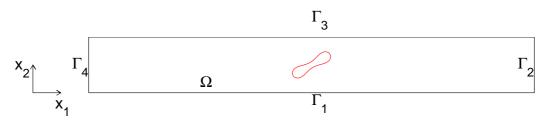


Figure 2: An example of the computational domain with a cell.

2.1. Elastic spring model for the RBC membrane

An elastic spring model used in [18] is considered in this paper to describe the deformable behavior of the RBCs. Based on this model, the RBC membrane can be viewed as membrane particles connecting with the neighboring membrane particles by springs, as shown in Fig. 3. Elastic energy stores in the spring due to the change of the length l of the spring with respected to its reference length l_0 and the change in angle

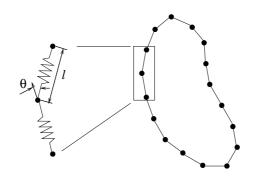


Figure 3: The elastic spring model of the RBC membrane.

 θ between two neighboring springs. The total elastic energy of the RBC membrane, $E = E_l + E_b$, is the sum of the total elastic energy for stretch/compression and the total energy for bending which, in particular, are

$$E_l = \frac{k_l}{2} \sum_{i=1}^{N} \left(\frac{l_i - l_0}{l_0}\right)^2$$
(2.6)

and

$$E_b = \frac{k_b}{2} \sum_{i=1}^{N} \tan^2(\theta_i/2).$$
(2.7)

In Eqs. (2.6) and (2.7), N is the total number of the spring elements, and k_l and k_b are spring constants for changes in length and bending angle, respectively. (Another form of bending energy similar to the one in (2.7) can be found in [19].)

Remark 2.1. In the process of creating the initial shape of RBCs described in [18], the RBC is assumed to be a circle of radius $R_0 = 2.8 \ \mu m$ initially. The circle is discretized into N = 76 membrane particles so that 76 springs are formed by connecting the neighboring particles. The shape change is stimulated by reducing the total area of the circle through a penalty function

$$\Gamma_s = \frac{k_s}{2} \left(\frac{s - s_e}{s_e}\right)^2,\tag{2.8}$$

where s and s_e are the time dependent area of the RBC and the specified equilibrium area of the RBC, respectively, and the total energy is modified as $E + \Gamma_s$. Based on the principle of virtual work the force acting on the *i*th membrane particle now is

$$\mathbf{F}_{i} = -\frac{\partial(E + \Gamma_{s})}{\partial \mathbf{r}_{i}},\tag{2.9}$$

where \mathbf{r}_i is the position of the *i*th membrane particle. When the area is reduced, each RBC membrane particle moves on the basis of the following equation of motion:

$$m\ddot{\mathbf{r}}_i + \gamma \dot{\mathbf{r}}_i = \mathbf{F}_i. \tag{2.10}$$

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Here, () denotes the time derivative; m and γ represent the membrane particle mass and the membrane viscosity of the RBC. The position \mathbf{r}_i of the *i*th membrane particle is solved by discretizing (2.10) via a second order finite difference method. The total energy stored in the membrane decreases as the time elapses. The final shape of the RBC is obtained as the total elastic energy is minimized (please see [20]). The area of the final shape has less than 0.001% difference from the specified equilibrium area s_e and the length of the perimeter of the final shape has less than 0.005% difference from the circumference of the initial circle. The reduced area of a RBC in this paper is defined by $s^* = s_e/\pi R_0^2$.

Remark 2.2. When simulating the case involving a moving interface, we have applied a repulsive force to prevent the overlapping between cell and wall. The repulsive force is obtained from the following Morse potential, $\phi(d) = k_r (1 - e^{-(d-d_0)})^2$, (e.g., see [21]) where the parameter *d* is the shortest distance between the membrane particle and the wall and d_0 is the range of the repulsive force so that

$$f_i(d) = \begin{cases} 2k_r(1 - e^{-(d-d_0)})e^{-(d-d_0)}, & d \le d_0, \\ 0, & d > d_0, \end{cases}$$

i.e., when the distance d is greater than d_0 , there is no repulsive force. The parameter k_r is a constant for the strength of the potential. To save the cost of computing the repulsive force in simulations, each cell is covered by a disk whose center is the cell mass center and the repulsive force at each membrane particle is computed only if the distance from the disk center to the wall is less than the sum of the disk radius and the range of the repulsive force.

2.2. Immersed boundary method

The immersed boundary method developed by Peskin, e.g., [5–7], is employed in this study because of its distinguish features in dealing with the problem of fluid flow interacting with a flexible fluid/structure interface. Over the years, it has demonstrated its capability in study of computational fluid dynamics including blood flow. Based on the method, the boundary of the deformable structure is discretized spatially into a set of boundary nodes. The force located at the immersed boundary node $\mathbf{r}_i = (r_{i,1}, r_{i,2})$ affects the nearby fluid mesh nodes $\mathbf{x} = (x_1, x_2)$ through a 2D discrete δ -function $D_h(\mathbf{x} - \mathbf{r}_i)$:

$$\mathbf{f}(\mathbf{x}) = \sum \mathbf{F}_i D_h(\mathbf{x} - \mathbf{r}_i) \quad \text{for } |\mathbf{x} - \mathbf{r}_i| \le 2h,$$
(2.11)

where h is the uniform finite element mesh size and

$$D_h(\mathbf{x} - \mathbf{r}_i) = \delta_h(x_1 - r_{i,1})\delta_h(x_2 - r_{i,2}), \qquad (2.12)$$

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with the 1D discrete δ -functions being

$$\delta_{h}(z) = \begin{cases} \frac{1}{8h} \left(3 - 2|z|/h + \sqrt{1 + 4|z|/h - 4(|z|/h)^{2}} \right), & |z| \le h, \\ \frac{1}{8h} \left(5 - 2|z|/h - \sqrt{-7 + 12|z|/h - 4(|z|/h)^{2}} \right), & h \le |z| \le 2h, \\ 0, & \text{otherwise.} \end{cases}$$
(2.13)

The velocity of the immersed boundary node \mathbf{r}_i is also affected by the surrounding fluid and therefore is enforced by summing the velocities at the nearby fluid mesh nodes \mathbf{x} weighted by the same discrete δ -function:

$$\mathbf{U}(\mathbf{r}_i) = \sum h^2 \mathbf{u}(\mathbf{x}) D_h(\mathbf{x} - \mathbf{r}_i) \quad \text{for } |\mathbf{x} - \mathbf{x}_i| \le 2h.$$
 (2.14)

After each time step, the position of the immersed boundary node is updated by

$$\mathbf{r}_i^{n+1} = \mathbf{r}_i^n + \Delta t \mathbf{U}(\mathbf{r}_i^n). \tag{2.15}$$

2.3. Space approximation and time discretization

Concerning the finite element based space approximation of $\{\mathbf{u}, p\}$ in problem (2.1)-(2.5), we use the P_1 -iso- P_2 and P_1 finite element approximation (e.g., see [22, Chapter 5]). For a rectangular computational domain $\Omega \subset R^2$, let \mathcal{T}_h be a finite element triangulation of $\overline{\Omega}$ for velocity and \mathcal{T}_{2h} a twice coarser triangulation for pressure where h is a space discretization step. We introduce the finite dimensional spaces:

$$\begin{split} W_h &= \{ \mathbf{v}_h \, | \, \mathbf{v}_h \in C^0(\overline{\Omega})^2, \mathbf{v}_h |_T \in P_1 \times P_1, \forall T \in \mathcal{T}_h \}, \\ W_{0h} &= \{ \mathbf{v}_h \, | \, \mathbf{v}_h \in W_h, \mathbf{v}_h = \mathbf{0} \ \text{ on } \Gamma_d \}, \\ L_h^2 &= \{ q_h \, | \, q_h \in C^0(\overline{\Omega}), q_h |_T \in P_1, \forall T \in \mathcal{T}_{2h} \}, \\ L_{h,0}^2 &= \left\{ q_h \, | \, q_h \in L_h^2, \int_{\Omega} q_h \, d\mathbf{x} = 0 \right\}, \end{split}$$

where P_1 is the space of polynomials in two variables of degree ≤ 1 . We apply the *Lie's* scheme [22, 23], which is a first order method in time, with the above finite elements to Eqs. (2.1)-(2.5) with the backward Euler method in time for some subproblems and obtain the following sequence of fractional step subproblems (some of the subscripts *h* have been dropped):

 $\mathbf{u}^0 = \mathbf{u}_0$ is given; for $n \ge 0$, \mathbf{u}^n being known, we compute the approximate solution via the following fractional steps:

1. Update the position of the membrane by (2.14) and (2.15) and then compute the force f^n based on the fluid/cell interface by (2.9) and (2.11).

2. Solve

$$\begin{cases} \int_{\Omega} \frac{\partial \mathbf{u}(t)}{\partial t} \cdot \mathbf{v} d\mathbf{x} + \int_{\Omega} (\mathbf{u}^{n} \cdot \nabla) \mathbf{u}(t) \cdot \mathbf{v} d\mathbf{x} = 0, & \text{on } (t^{n}, t^{n+1}), \forall \mathbf{v} \in W_{0h}^{-}, \\ \mathbf{u}(t^{n}) = \mathbf{u}^{n}, \\ \mathbf{u}(t) \in W_{h}, \ \mathbf{u}(t) = \mathbf{g}_{0,h} & \text{on } \Gamma^{-} \times (t^{n}, t^{n+1}), \end{cases}$$
(2.16)

and set $u^{n+2/3} = u(t^{n+1})$.

3. Finally solve

$$\begin{cases} \rho \int_{\Omega} \frac{\mathbf{u}^{n+1} - \mathbf{u}^{n+2/3}}{\Delta t} \cdot \mathbf{v} d\mathbf{x} + \mu \int_{\Omega} \nabla \mathbf{u}^{n+1} : \nabla \mathbf{v} d\mathbf{x} \\ - \int_{\Omega} p^{n+1} (\nabla \cdot \mathbf{v}) d\mathbf{x} = \int_{\Omega} \mathbf{f}^{n} \cdot \mathbf{v} d\mathbf{x}, \quad \forall \mathbf{v} \in W_{0h}, \\ \int_{\Omega} q \nabla \cdot \mathbf{u}^{n+1} d\mathbf{x} = 0, \quad \forall q \in L_{h}^{2}, \\ \mathbf{u}^{n+1} \in W_{h}, \quad \mathbf{u}^{n+1} = \mathbf{g}_{0,h} \quad \text{on } \Gamma_{d}; \quad p^{n+1} \in L_{h}^{2} \ (p^{n+1} \in L_{h,0}^{2} \quad \text{if } \Gamma_{n} = \emptyset). \end{cases}$$
(2.17)

In Eq. (2.16), we have $\Gamma^- = \{\mathbf{x} \mid \mathbf{x} \in \Gamma, \mathbf{g}_{0,h}(\mathbf{x}) \cdot \mathbf{n}(\mathbf{x}) < 0\}$ and $W_{0h}^- = \{\mathbf{v}_h \mid \mathbf{v}_h \in W_h, \mathbf{v}_h = \mathbf{0} \text{ on } \Gamma^-\}$. The quasi-Stokes problem (2.17) is solved by a preconditioned conjugate gradient method (see, e.g., [22]). The subproblem (2.16) is an advection type subproblem. It is solved by a wave-like equation method, which is described in detail in [24] and [25].

Remark 2.3. In simulations, the computational domain Ω moves to the right with either the mass center of a RBC or the interface (see, e.g., [26,27] and references therein for adjusting the computational domain according to the position of the particle). Due to the use of structured and uniform mesh in our simulations, it is relatively easy to have the computational domain moving with either a designated cell or an moving interface without the need of generating any new meshes. Here is the general idea: When the mass center of a RBC moves to the right in an infinitely long channel, we add one vertical grid line to the right end of the computational domain. In the same time we drop one vertical grid line at the left end of the computational domain. In the meantime at these new grid points added at the right end, we assign the values of an undisturbed field according to either Poiseuille flow or simple shear flow depending on the flow condition. When following an interface moving to the right with a constant speed, we have applied the same strategy. The comparison of the simulation results associated with different boundary conditions are discussed in the following section.

3. Numerical results and discussion

3.1. Tank-treading of a single cell in shear flow

We have first validated the computational methodology with two types of boundary conditions discussed in Section 2 by comparing the inclination angle and the tanktreading frequency of a single RBC in shear flow. The values of parameters for modeling cells are same with [15–17] as follows: The bending constant is $k_b = 5 \times 10^{-10} \text{N} \cdot \text{m}$, the spring constant is $k_l = 5 \times 10^{-8} \text{N} \cdot \text{m}$, the penalty coefficient is $k_s = 10^{-5} \text{N} \cdot \text{m}$, the repulsive force coefficient is $k_r = 10^{-9} \text{N} \cdot \text{m}$, and the range of the repulsive force is $d_0 = 2h$ where h is the mesh size for the flow velocity field. The cells are suspended in blood plasma which has a density $\rho = 1.00 \text{g/cm}^3$ and a dynamical viscosity $\mu = 0.012 \text{g/(cm \cdot s)}$. The viscosity ratio which describes the viscosity contrast of the inner and outer fluid of the RBC membrane is fixed at 1.0. The dimensions of the computational domain are $112\mu m \times 7\mu m$ (the longer domain) and $80\mu m \times 7\mu m$ (the shorter domain). Then the degree of confinement $(2R_0/H)$ is 0.8 where H is the height of the channel. The grid resolution for the computational domain is 80 grid points per $10\mu m$. The time step Δt is 1×10^{-5} ms. The initial position of the mass center of the cells are (56, 3.5) and (40, 3.5) for the longer domain and the shorter domain, respectively. To have a shear flow, a Couette flow driven by two walls at the top and bottom which have the same speed U/2 but move in directions opposite to each other is applied to the suspension, where the speed U is given by $U = \gamma * H$ with a given shear rate γ . The shear rate used in the simulation is $\gamma = 275/s$. The steady inclination angles of the tank-treading for four values of $s^*=0.6$, 0.7, 0.8 and 0.9 are presented in Fig. 4, which show the very good agreement with the lattice-Boltzmann simulation results

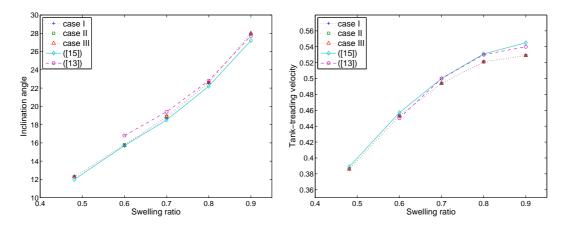


Figure 4: (Color online). Steady inclination angle versus the cell swelling ratio (left) and membrane tank-treading velocity (scaled by $\gamma R_0/2$) versus the cell swelling ratio (right) in comparison to Shi et al. [15] and Kaoui et al. [13] in different cases. Case I: $112\mu m \times 7\mu m$ domain with Dirichlet boundary conditions, Case II: $80\mu m \times 7\mu m$ domain with Neumann inflow condition and Dirichlet outflow condition.

in [13] and those previously obtained with periodic boundary conditions in [15]. The membrane tank-treading velocity (scaled by $\gamma R_0/2$) is also in good agreement with the results in [13, 15]. In Fig. 4, the results of the inclination angle and the tank-treading velocity are almost the same when having either the Dirichlet boundary conditions on Γ with the length L = 112 and 80 μ m or the conditions (2.3) and (2.4) on the boundary of the shorter domain. For the above single-cell validation, the maximal relative change of the spring length during the simulation, $\max_{1 \le i \le N} |l_i - l_0|/l_0$, is less than 0.01%, which shows that the cell is almost inextensible.

3.2. Multi-cell aggregation in a capillary behind a moving interface

For the cases involving a moving interface in a capillary, we have considered the one moving to the right with constant speed U to mimic the motion of the RBCs behind a meniscus in a capillary. Then the associated boundary condition in (2.3) on Γ_d is $\mathbf{g}_0 = \mathbf{0}$ on $\Gamma_1 \cup \Gamma_3$ and $\mathbf{g}_0 = (U, 0)^t$ on Γ_2 and the boundary condition (2.4) is satisfied on Γ_4 . We have kept all the related parameters the same except the following. We have first considered the case of 12 cells of swelling ratio $s^*=0.481$ in a capillary of the height 10 μ m. The computational domain Ω is 80μ m \times 10 μ m. The grid resolutions for the computational domain are 64 and 80 grid points per $10\mu m$. The interface speed is U = 8/3 cm/s. In the simulation, the cells at the central region of the channel move faster than those next to the top and bottom walls do due to fact that the velocity field behaves like Poiseuille flow as the fluid flow is away from the interface and the speed of the interface is slower than the velocity of the fluid flow in the channel central region away from the interface (see the velocity field in Figs. 5 and 6). Thus the cells in the central region are piled up behind the interface while those next to the walls migrate toward the central region (as the cell in red in Fig. 5). Then the cells form a slug behind the moving interface and move with the interface as in Fig. 5. The position and shape of the cells obtained with two different mesh sizes are about the same for the first 4 ms as in Fig. 5 and then they become different since the effect of the round-off errors and approximation errors can kick in. For the above case of 12 cells, the maximal relative change of the spring length during the simulation, $\max_{1 \le i \le N} |l_i - l_0|/l_0$, is less than 0.5% but slightly larger than the one of one cell case due to the strong interaction among cells in the region of slug. For the case of 68 cells of swelling ratio $s^* = 0.481$ in a capillary of the height $20\mu m$, we have considered the computational domain $\Omega =$ $160\mu m \times 20\mu m$. The interface speed is U = 8/3 cm/s. These 68 cells behave similarly behind the moving interface like the motion of the 12 cells considered in the previous case. But it is much clearly for us to see that the cells in the channel central region move faster to the right due to the relatively faster flow field. For the cells moving away from the interface, they move back to the central region of the channel due to either the interaction among the cells or the lateral migration of the cells in a flow field like the Poiseuille flow. Then the cells are piled up behind the interface and move with the interface as in Fig. 6.

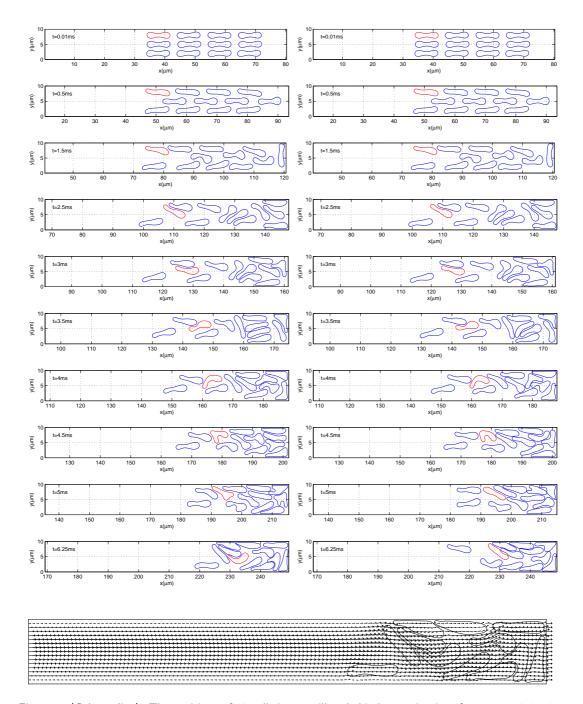


Figure 5: (Color online). The positions of 12 cells in a capillary behind a moving interface at t = 0.01, 0.5, 1.5, 2.5, 3, 3.5, 4, 4.5, 5 and 6.25 ms (from top to bottom) obtained with the mesh size 64 grid points per 10μ m (left column) and 80 grid points per 10μ m (right column). The velocity field with 12 cells at t = 6.25 ms is obtained with the mesh size 64 grid points per 10μ m. The position of the "red" cell shows its lateral migration toward the central region.

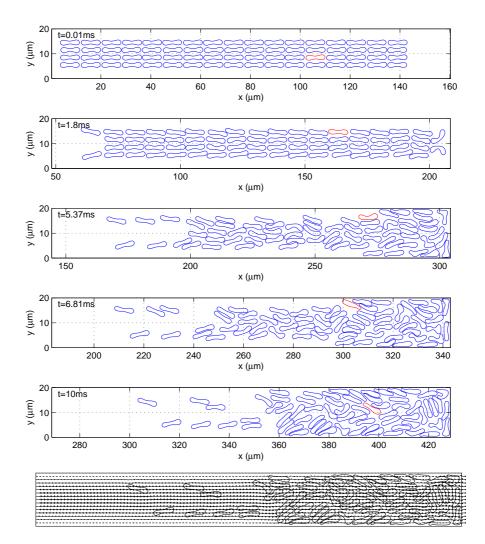


Figure 6: (Color online). The position of 68 cells in a capillary behind a moving interface at t = 0.01, 1.8, 5.37, 6.81 and 10 ms and the velocity field with 68 cells at t = 10 ms (from top to bottom). The position of the "red" cell shows its lateral migration toward the central region.

4. Conclusions

In summary, we have developed computational modeling and methodologies for simulating the motion of many RBCs in a capillary behind a moving interface in this paper. The methodology is based on an immersed boundary method and the skeleton structure of the red blood cell (RBC) membrane is modeled as a spring network. The computational domain is moving with either a designated RBC or an interface in an infinitely long two-dimensional channel with an undisturbed flow field in front of the domain. The tanking-treading and the inclination angle of a cell in a simple shear flow are briefly discussed for the validation purpose. The results of the motion of red blood cells behind a moving interface in a capillary show that the RBCs with higher velocity than the interface speed form a concentrated slug behind the interface, which is consistent with the results in [1,2]. The lateral migration is a also key factor for the formation of a slug behind the moving interface. For the cases in which the swelling ratio of cells or the marching velocities are different, the cells should behave similarly as the simulating results since the they all behave similarly in Poiseuille flow.

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